CLAIMS

- 1) Catalytic composition comprising gallium, at least one element chosen in the group of the lanthanides and a zeolite belonging to the MFI, MEL or MFI/MEL families, the crystal lattice of which is made up of silicon oxide and at least one metal oxide chosen from among aluminium oxide, boron oxide and gallium oxide.
- 2) A composition according to Claim 1, in which the zeolite is chosen from among ZSM-5, zeolites having an MFI structure based on silicon oxide, gallium oxide and possibly aluminium oxide, zeolites having an MFI structure based on silicon oxide and boron oxide, ZSM-11, zeolites having a MEL structure based on silicon oxide and boron oxide, ZSM-8, and zeolites having an MFI/MEL structure based on silicon oxide and boron oxide.
 - 3) A composition according to Claim 2, in which the zeolite is ZSM-5.
- 20 4) A catalytic composition according to Claim
 1, in which the molar ratio between silica and the
 metal oxide is greater than 20.
- 5) A catalytic composition according to Claim
 4, in which the molar ratio between silicon oxide
 25 and metal oxide is greater than 20 and less than

500.

- 6) A catalytic composition according to Claim 5, in which the molar ratio between silicon oxide and metal oxide is greater than 20 and less than or equal to 70.
- 7) A catalytic composition according to Claim 6, in which the molar ratio between silicon oxide and metal oxide is greater than 20 and less than 60.
- 10 8) A catalytic composition according to Claim
 1, comprising gallium, at least one element chosen
 in the group of the lanthanides and a zeolite
 belonging to the MFI family characterized by
 crystallites which for at least 90% have diameters
 15 smaller than 500 Å.
 - 9) A catalytic composition according to Claim 8, in which the MFI zeolite consists of crystallites with diameters smaller than 500 Å.
- 10) A catalytic composition according to Claim
 20 8, in which the crystallites of the MFI zeolite
 present in the form of mulberry-shaped submicron
 aggregates with an extrazeolitic porosity of a
 meso-macroporous nature.
- 11) A catalytic composition according to Claim25 10, in which the total volume of said extrazeolitic

porosity consists for at least 30% of pores with diameters of less than 500 $\hbox{\normalfont\AA}$.

- 12) A catalytic composition according to Claim 8, in which the crystal lattice of the MFI zeolite is made up of silicon oxide and aluminium oxide.
- 13) A catalytic composition according to Claim
 12, in which the molar ratio between silicon oxide
 and aluminium oxide is greater than 20.
- 14) A catalytic composition according to Claim
 10 13, in which the molar ratio between silicon oxide
 and aluminium oxide is greater than 20 and less
 than 500.
- 15) A catalytic composition according to Claim 14, in which the molar ratio between silicon oxide and aluminium oxide is greater than 20 and less than or equal to 100.
 - 16) A catalytic composition according to Claim 1 or Claim 8, in which the zeolite is partially in acid form.
- 20 17) A catalytic composition according to any one of the foregoing claims, containing, in addition, rhenium.
- 18) A catalytic composition according to Claim
 1, Claim 8 or Claim 17, in which the lanthanide is
 25 present in the form of an oxide, ion, metal, or is

a mixture of these forms.

- 19) A catalytic composition according to Claim

 1, Claim 8 or Claim 17, in which the amount of
 lanthanide, expressed as element, ranges from 0.01
 to 10 wt%.
 - 20) A catalytic composition according to Claim
 19, in which the amount of lanthanide, expressed as
 element, ranges from 0.1 to 2 wt%.
- 21) A catalytic composition according to Claim

 10 1, Claim 8 or Claim 17, in which the lanthanide is chosen from among neodymium and lanthanium, either alone or in mixtures with cerium and/or praseodymium, and mixtures of neodymium and lanthanium, possibly also containing cerium and/or praseodymium.
 - 22) A catalytic composition according to Claim

 1, Claim 8 or Claim 17, in which the gallium is

 present in the form of an oxide, gallium ion,

 metallic gallium, or is a mixture of said forms.
- 23) A catalytic composition according to Claim
 1, Claim 8 or Claim 17, in which the amount of
 gallium, expressed as element, ranges from 0.05 to
 10 wt%.
- 24) A catalytic composition according to Claim
 25 23 ,in which the amount of gallium, expressed as

element, ranges from 0.5 to 4 wt%.

- 25) A catalytic composition according to Claim 17, in which the amount of rhenium, expressed as element, ranges from 0.05 to 10 wt% with respect to the total weight of the catalytic composition.
- 26) A catalytic composition according to Claim 25, in which the amount of rhenium ranges from 0.5 to 4 wt%.
- 27) A catalytic composition according to Claim 10 17, in which the rhenium is present in the form of an oxide, ion, metal, or is a mixture of said forms.
- 28) A catalytic composition according to Claim

 1, Claim 8 or Claim 17, containing a binder chosen

 15 from among silica, alumina and clay, in a proportion by weight ranging from 50:50 to 95:5.
 - 29) A catalytic composition according to Claim 8 or Claim 12, in which the zeolite is prepared by subjecting to vigorous stirring a solution containing sources of tetra-propyl-ammonium ion, sodium oxide, aluminium oxide, silicon oxide, and water, having the following composition expressed as molar ratios:

OH⁻free/SiO2 0.07-1.0

25 $(C_3H_7)_4N^+/SiO_2 0.01-1$

H₂O/OH⁻free 10-300

 $SiO_2/Al_2O_3 > 5$

 Na^{+}/SiO_{2} 0.6-5

up to completion of crystallization.

30) A catalytic composition according to Claim 29, in which the composition of the synthesis mixture is the following:

 OH_{free}/SiO_2 0.1-0.3

 $(C_3H_7)_4N^+/SiO_2$ 0.05-0.25

 H_2O/OH_{free} 20-60

 SiO_2/Al_2O_3 50-120

 Na^+/SiO_2 1-4

- 31) Composition according to Claim 29, in which the crystallization is performed at a 15 temperature in the range from 90 to 130°C, under stirring for a time which ranges from 3 hours to 15 days, and possibly comprises a second stage that can last up to 5 days in which the temperature is raised to a value ranging from 110 to 160°C.
- 20 32) Composition according to Claim 29, in which the source of the tetra-propyl-ammonium ion is chosen from among the corresponding bromide or hydroxide or tri-n-propylammine in mixture with n-propyl bromide.
- 25 33) Composition according to Claim 29, in

which the source of silicon oxide is chosen from among sodium silicate, silica hydrosol, silica gel, and silicic acid.

- Composition according to Claim 29, which the source of aluminium oxide is chosen from aluminate, aluminium sodium alumina, among sulphate, and aluminium nitrate.
- 35) Composition according to Claim 29, which the source of sodium is chosen from among the corresponding hydroxide, halides, sulphate and/or 10 from among the sources of aluminium and/or silicon which contain it.
 - for preparing the catalytic A process compositions according to Claim 1 or Claim 8, which comprises treating the zeolite with a gallium compound, treating the product thus obtained with a lanthanide compound, drying and calcining.
 - 37) A process for preparing the catalytic composition according to Claim 1 or Claim 8, which comprises treating the zeolite with a lanthanide compound, treating the product thus obtained with a gallium compound, drying and calcining, or else treating the zeolite with a mixture comprising a gallium compound and a lanthanide compound, drying

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- 38) A process according to Claim 36 or Claim 37, in which the zeolite is in acid form.
- 39) A process according to Claim 36, Claim 37 or Claim 38, in which the treatment with a gallium compound and the treatment with a lanthanide compound are chosen from between ion exchange and impregnation.

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- 40) A process according to Claim 39, in which ion exchange and impregnation are performed using an aqueous solution of a gallium salt and an aqueous solution of a lanthanide salt.
 - 41) A process according to Claim 39 or Claim 40, in which the treatment with a gallium compound consists in an ion exchange or impregnation with an aqueous solution of a gallium salt, and the treatment with a lanthanide compound consists in an impregnation with an aqueous solution of a lanthanide salt.
- 42) A process according to Claim 40, in which
 20 the gallium salt and the lanthanide salt are chosen
 from among the corresponding nitrates, chlorides
 and sulphates.
 - 43) A process according to Claim 36 or Claim
 41, which comprises the treatment of the zeolite by
 means of ion exchange or impregnation with an

aqueous solution of a gallium salt, drying, possibly calcining the resulting product, treating it by means of impregnation with an aqueous solution of a lanthanide salt, drying and calcining.

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- 44) A process for preparing the catalytic composition according to Claim 17, which comprises treating the zeolite with a gallium compound, a lanthanide compound and a rhenium compound, in any order, drying and calcining.
- 45) A process according to Claim 44, which comprises: a) the treatment of the zeolite by means of ion exchange or impregnation with an aqueous solution of a gallium salt, drying, and possibly calcining the resulting product; b) treating it by means of impregnation with an aqueous solution of a lanthanide salt, drying and possibly calcining the resulting product; and c) treating it by means of impregnation with an aqueous solution of a rhenium salt, drying and calcining.
- 46) A process for the production of aromatic hydrocarbon compounds which comprises setting in contact one or more aliphatic hydrocarbons containing from 3 to 6 carbon atoms with a catalytic composition comprising gallium, at least

one element chosen in the group of the lanthanides, a zeolite belonging to the MFI, MEL or MFI/MEL families, the crystal lattice of which is made up of silicon oxide and at least one metal oxide chosen from among aluminium oxide, boron oxide and gallium oxide.

- 47) A process according to Claim 46, in which the zeolite is ZSM-5.
- 48) A process according to Claim 46, in which

 10 the molar ratio between silicon oxide and metal

 oxide is greater than 20.
 - 49) A process according to Claim 48, in which the molar ratio between silicon oxide and metal oxide is greater than 20 and less than 500.
- 15 50) A process according to Claim 49, in which the ratio between silicon oxide and metal oxide is greater than 20 and less than or equal to 70.
 - 51) A process according to Claim 50, in which the ratio between silicon oxide and metal oxide is greater than 20 and less than 60.

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52) A process according to Claim 46, in which the catalytic composition comprises gallium, at least one element chosen in the group of the lanthanides and a zeolite belonging to the MFI family characterized by crystallites which for at

least 90% have diameters smaller than 500 Å.

- 53) A process according to Claim 52, in which the MFI zeolite consists of crystallites with diameters smaller than 500 Å.
- 54) A process according to Claim 52, in which the crystallites of MFI zeolite present in the form of mulberry-shaped submicron aggregates with an extrazeolitic porosity of a meso-macroporous nature.
- 10 55) A process according to Claim 54, in which the total volume of said extrazeolitic porosity consists for at least 30% of pores with diameters of less than 500 Å.
- 56) A process according to Claim 52, in which

 15 the crystal lattice of the MFI zeolite is made up

 of silicon oxide and aluminium oxide.
 - 57) A process according to Claim 56, in which the molar ratio between silicon oxide and aluminium oxide is greater than 20.
- 58) A process according to Claim 57, in which the molar ratio between silicon oxide and aluminium oxide is greater than 20 and less than 500.
 - 59) A process according to Claim 58, in which the molar ratio between silicon oxide and aluminium oxide is greater than 20 and less than or equal to

100.

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- 60) A process according to Claim 46 or Claim 52, in which the zeolite is partially in acid form.
- 61) A process according to Claim 46 or Claim 52, in which the catalytic composition in addition contains rhenium.
 - or Claim 61, in which the lanthanide is chosen from among neodymium and lanthanium, either alone or in mixture with cerium and/or praseodymium, and mixtures of neodymium and lanthanium, possibly containing cerium and/or praseodymium.
- 63) A process according to Claim 46, Claim 52 or Claim 61, in which the hydrocarbon or the aliphatic hydrocarbons are chosen from among olefins, cyclo-olefins, paraffins, and cycloparaffins.
- 64) A process according to Claim 46, Claim 52 or Claim 61, in which the hydrocarbon or the aliphatic hydrocarbons contain from 4 to 5 carbon atoms.
 - 65) A process according to Claim 63 or Claim 64, in which the aliphatic hydrocarbon is chosen from among n-pentane, n-pentenes, n-butane, n-butane, n-butane, iso-butane, methylbutenes,

cyclopentenes, isopentane, cyclopentane, or their mixtures.

- 66) A process according to Claim 46, Claim 52 or Claim 61, in which mixtures of aliphatic hydrocarbons are used containing from 20 to 90 wt% of olefins.
- 67) A process according to Claim 66, in which mixtures of aliphatic hydrocarbons are used containing from 40 to 70 wt% of olefins.
- 10 68) A process according to Claim 46, Claim 52 or Claim 61, conducted at a temperature ranging from 300° to 800° C, and at a pressure ranging from 0 to 20 barg.
- 69) A process according to Claim 68, conducted 15 at a temperature ranging from 400° to 650° C, and at a pressure ranging from 1 to 10 barg.
 - 70) A process according to Claim 68, conducted at a WHSV ranging from 0.1 to 30 hours⁻¹.